COURSE OVERVIEW PE0127
Operations Abnormalities & Plant Upset

Course Title
Operations Abnormalities & Plant Upset

Course Date/Venue
September 07-11, 2025/TBA Meeting Room, Hilton Kuwait Resort, Mangaf, Kuwait City, Kuwait

Course Reference
PE0127

Course Duration/Credits
Five days/3.0 CEUs/30 PDHs

Course Description

This practical and highly-interactive course includes various practical sessions and exercises. Theory learnt will be applied using our state-of-the-art simulators.

Managing Manpower effectively and assess risk properly during plant upset are key effective factors when reacting with incidents. Incidents may start minor and become major by wrong reaction and wrong decisions. The aim of this course is to make everybody involved in the operations know exactly what to do. The incident itself may cause a certain loss, but with wrong reaction it became a massive loss. Understanding operation, effective emergency/contingency plan, rules of each one within emergency plan and makes emergency tools ready and in operational condition are the main aims of this course. One approach to overcome any incident development is to prepare yourself and emergency team to treat incidents situation professionally.

Upon review of several incidents, two common causes were identified that contributed to those incidents. The causes are improper management of manpower during upset conditions and improper risk assessment of activities to be executed or stop doing. However, on close examination the trained emergency team and correct managing of the incident besides using correct emergency tools will minimize the loss and accidents consequences.

Effective training is the necessary foundation for the successful implementation of optimum emergency managing condition and optimum consequences minimizing. This course will train participants on managing risk & manpower during plant upset to save lives, assets and company reputations.

Course Objectives

Upon the successful completion of this course, each participant will be able to:-

- Manage manpower effectively and assess risk properly during the abnormalities of the operations and plant upset
- Assess staffing level in abnormal situations and distribute manpower during plant upset conditions
- Manage shift teams, assess risk of non-routine activities and manage operational crisis
- Identify risks in the process and describe the roles, responsibilities and procedures in emergency management
- Use the risk assessment process and have enough skills in monitoring and auditing the emergency tools
- Recognize the training requirements for process emergency handling including emergency team building
- Discuss the various skills that will be acquired in controlling emergency management using different scenarios and matrix
- Identify the common mistakes during emergencies and employ the preventive measures

Exclusive Smart Training Kit - H-STK®

*Participants of this course will receive the exclusive "Haward Smart Training Kit" (**H-STK®**). The **H-STK®** consists of a comprehensive set of technical content which includes **electronic version** of the course materials conveniently saved in a **Tablet PC**.*

Who Should Attend

This course provides an overview of all significant aspects and considerations of operations abnormalities and plant upset for superintendents, supervisors and foremen in various departments of process plants (production, operations, maintenance, utility, etc.). Further, the course is suitable for emergency teams, managers, supervisors and other technical staff.

Course Fee

US$ 5,500 per Delegate. This rate includes H-STK® (Haward Smart Training Kit), buffet lunch, coffee/tea on arrival, morning & afternoon of each day.

Course Certificate(s)

Internationally recognized certificates will be issued to all participants of the course who completed a minimum of 80% of the total tuition hours.

Certificate Accreditations

Certificates are accredited by the following international accreditation organizations: -

- The International Accreditors for Continuing Education and Training (IACET - USA)

  Haward Technology is an Authorized Training Provider by the International Accreditors for Continuing Education and Training (IACET), 2201 Cooperative Way, Suite 600, Herndon, VA 20171, USA. In obtaining this authority, Haward Technology has demonstrated that it complies with the **ANSI/IACET 2018-1 Standard** which is widely recognized as the standard of good practice internationally. As a result of our Authorized Provider membership status, Haward Technology is authorized to offer IACET CEUs for its programs that qualify under the **ANSI/IACET 2018-1 Standard**.

  Haward Technology's courses meet the professional certification and continuing education requirements for participants seeking **Continuing Education Units** (CEUs) in accordance with the rules & regulations of the International Accreditors for Continuing Education & Training (IACET). IACET is an international authority that evaluates programs according to strict, research-based criteria and guidelines. The CEU is an internationally accepted uniform unit of measurement in qualified courses of continuing education.

  Haward Technology Middle East will award **3.0 CEUs** (Continuing Education Units) or **30 PDHs** (Professional Development Hours) for participants who completed the total tuition hours of this program. One CEU is equivalent to ten Professional Development Hours (PDHs) or ten contact hours of the participation in and completion of Haward Technology programs. A permanent record of a participant's involvement and awarding of CEU will be maintained by Haward Technology. Haward Technology will provide a copy of the participant's CEU and PDH Transcript of Records upon request.

- British Accreditation Council (BAC)

  Haward Technology is accredited by the **British Accreditation Council** for **Independent Further and Higher Education** as an **International Centre**. BAC is the British accrediting body responsible for setting standards within independent further and higher education sector in the UK and overseas. As a BAC-accredited international centre, Haward Technology meets all of the international higher education criteria and standards set by BAC.

Accommodation

Accommodation is not included in the course fees. However, any accommodation required can be arranged at the time of booking.

Course Instructor(s)

This course will be conducted by the following instructor(s). However, we have the right to change the course instructor(s) prior to the course date and inform participants accordingly:

Mr. Mervyn Frampton is a **Senior Process Engineer** with over **30 years** of industrial experience within the **Oil & Gas**, **Refinery**, **Petrochemical** and **Utilities** industries. His expertise lies extensively in the areas of **Process Troubleshooting**, **Distillation Towers**, **Fundamentals of Distillation** for Engineers, **Distillation** Operation and Troubleshooting, **Advanced Distillation** Troubleshooting, **Distillation** Technology, Vacuum **Distillation**, **Distillation Column** Operation & Control, **Oil Movement** Storage & Troubleshooting, **Process Equipment** Design, Applied **Process Engineering** Elements, **Process Plant** Optimization, **Revamping & Debottlenecking**, **Process Plant** Troubleshooting & Engineering Problem Solving, **Process Plant** Monitoring, **Catalyst** Selection & Production Optimization, Operations Abnormalities & Plant Upset, **Process Plant** Start-up & Commissioning, **Clean Fuel** Technology & Standards, Flare, Blowdown & Pressure Relief Systems, **Oil & Gas Field Commissioning** Techniques, **Pressure Vessel** Operation, **Gas Processing**, **Chemical** Engineering, **Process Reactors** Start-Up & Shutdown, **Gasoline Blending** for Refineries, **Urea Manufacturing** Process Technology, Continuous Catalytic Reformer (**CCR**), **De-Sulfurization** Technology, Advanced Operational & Troubleshooting Skills, Principles of Operations Planning, **Rotating Equipment** Maintenance & Troubleshooting, **Hazardous Waste Management & Pollution Prevention**, **Heat Exchangers & Fired Heaters** Operation & Troubleshooting, **Energy Conservation** Skills, **Catalyst Technology**, **Refinery & Process Industry**, **Chemical Analysis**, **Process Plant**, **Commissioning & Start-Up**, **Alkylation**, **Hydrogenation**, **Dehydrogenation**, **Isomerization**, **Hydrocracking & De-Alkylation**, **Fluidized Catalytic Cracking**, **Catalytic Hydrodesulphuriser**, **Kerosene Hydrotreater**, **Thermal Cracker**, **Catalytic Reforming**, **Polymerization**, **Polyethylene**, **Polypropylene**, Pilot Water Treatment Plant, **Gas Cooling**, **Cooling Water Systems**, Effluent Systems, Material Handling Systems, **Gasifier**, **Gasification**, Coal Feeder System, **Sulphur Extraction Plant**, **Crude Distillation Unit**, **Acid Plant Revamp** and **Crude Pumping**. Further, he is also well-versed in HSE Leadership, Project and Programme Management, Project Coordination, Project Cost & Schedule Monitoring, Control & Analysis, Team Building, Relationship Management, Quality Management, Performance Reporting, Project Change Control, Commercial Awareness and Risk Management.

During his career life, Mr. Frampton held significant positions as the **Site Engineering Manager**, **Senior Project Manager**, **Process Engineering Manager**, **Project Engineering Manager**, **Construction Manager**, **Site Manager**, **Area Manager**, **Procurement Manager**, **Factory Manager**, **Technical Services Manager**, **Senior Project Engineer**, **Process Engineer**, **Project Engineer**, **Assistant Project Manager**, **Handover Coordinator** and **Engineering Coordinator** from various international companies such as the **Fluor Daniel**, **KBR** South Africa, **ESKOM**, MEGAWATT PARK, CHEMEPIC, PDPS, CAKASA, **Worley Parsons**, Lurgi South Africa, **Sasol**, **Foster Wheeler**, **Bosch** & **Associates**, **BCG** Engineering Contractors, Fina Refinery, Sapref Refinery, Secunda Engine Refinery just to name a few.

Mr. Frampton has a **Bachelor degree** in **Industrial Chemistry** from **The City University** in **London**. Further, he is a **Certified Instructor/Trainer**, a **Certified Internal Verifier/Trainer/Assessor** by the **Institute of Leadership & Management** (**ILM**) and has delivered numerous trainings, courses, workshops, conferences and seminars internationally..

Training Methodology

All our Courses are including **Hands-on Practical Sessions** using equipment, State-of-the-Art Simulators, Drawings, Case Studies, Videos and Exercises. The courses include the following training methodologies as a percentage of the total tuition hours:-

30% Lectures
20% Practical Workshops & Work Presentations
30% Hands-on Practical Exercises & Case Studies
20% Simulators (Hardware & Software) & Videos

In an unlikely event, the course instructor may modify the above training methodology before or during the course for technical reasons.

Course Program

The following program is planned for this course. However, the course instructor(s) may modify this program before or during the course for technical reasons with no prior notice to participants. Nevertheless, the course objectives will always be met:

Day 1: Sunday, 07th of September 2025

0730 –0800	Registration & Coffee
0800 – 0815	Welcome & Introduction
0815 – 0830	**PRE-TEST**
0830 – 0930	**Introduction**
0930 – 0945	Break
0945 – 1100	**Understanding Operational Principles & Why Plants Get Upset**
1100 – 1230	**Roles & Responsibilities**
1230 – 1245	Break
1245 – 1420	**Emergency Team Buildings & Responsibilities of Each Member – Case Study**
1420 – 1430	**Recap**
1430	Lunch & End of Day One

Day 2: Monday, 08th of September 2025

0730 – 0900	**How Incidents Develop & Common Reasons**
0900 – 0915	Break
0915 – 1100	**Review of Several Incidents** Two Common Causes were Identified that Contributed to those Incidents
1100 – 1230	**Improper Management of Manpower During Upset Conditions**
1230 – 1245	Break
1245 – 1420	**Improper Management of Manpower During Upset Conditions (cont'd)**
1420 – 1430	**Recap**
1430	Lunch & End of Day Two

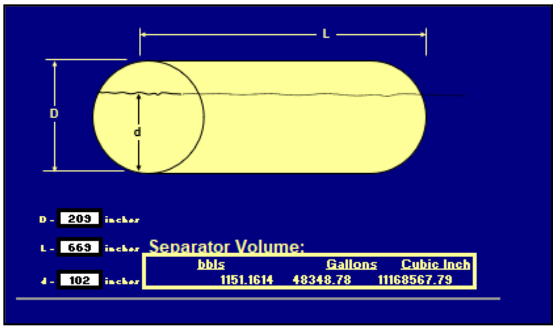
Day 3:	Tuesday, 09th of September 2025
0730 – 0930	**Root Cause Analysis (RCA)**
0930 – 0945	Break
0945 – 1100	**Risk Register**
1100 – 1215	**Incidents Development Scenarios – Discussion**
1215 – 1230	Break
1230 – 1420	**Incidents Development Scenarios – Discussion (cont'd)**
1420 – 1430	**Recap**
1430	Lunch & End of Day Three

Day 4:	Wednesday, 10th of September 2025
0730 – 0930	**Emergency Team Building & Improper Management of Manpower During Upset Conditions**
0930 – 0945	Break
0945 – 1100	**Improper Risk Assessment of Operation Conditions During Plant Upset**
1100 – 1215	**Risk Assessment & Risk Evaluation** Risk Matrix
1215 – 1230	Break
1230 – 1420	**Recognizing Key Points & Controlling Elements in Different Process**
1420 – 1430	**Recap**
1430	Lunch & End of Day Four

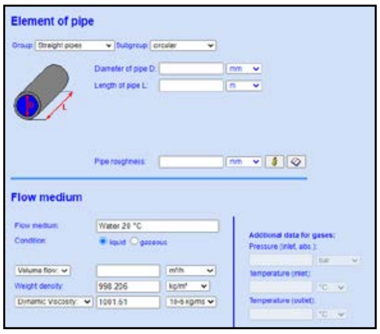
Day 5:	Thursday, 11th of September 2025
0730 – 0930	**Building Successful Emergency Team & Each One Roles & Responsibilities**
0930 – 0945	Break
0945 – 1100	**Closing Gaps & Correcting Scenarios**
1100 – 1215	**Closing Gaps & Correcting Scenarios (cont'd)**
1215 – 1230	Break
1230 – 1345	**Case Study & Discussion**
1345 – 1400	**Course Conclusion**
1400 – 1415	**POST-TEST**
1415 – 1430	Presentation of Course Certificates
1430	Lunch & End of Course

Simulator (Hands-on Practical Sessions)

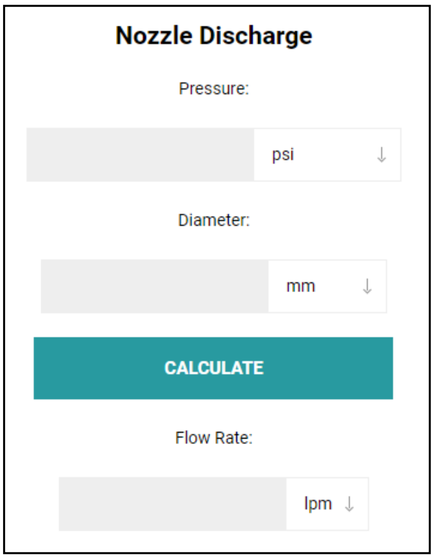
Practical sessions will be organized during the course for delegates to practice the theory learnt. Delegates will be provided with an opportunity to carryout various exercises using various online system calculator.



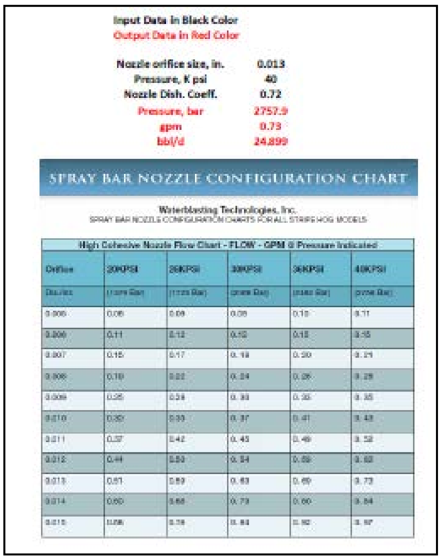
Tank Volume Calculator



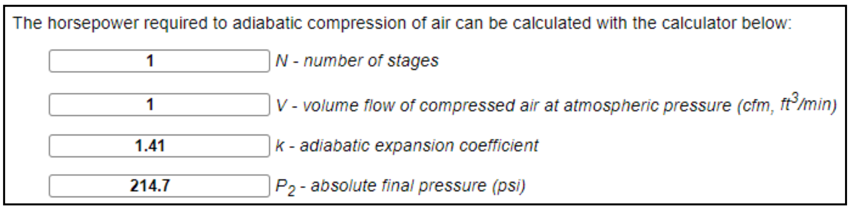
Pressure Drop Online-Calculator



Nozzle Discharge

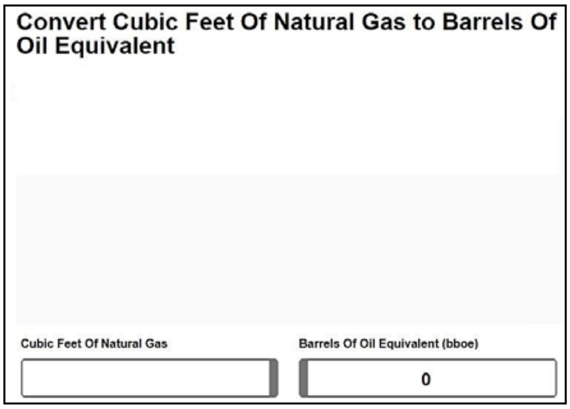


Nozzle Calculator

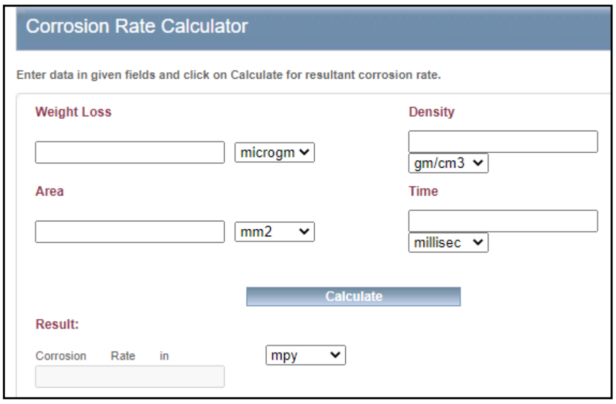


Horsepower Calculator

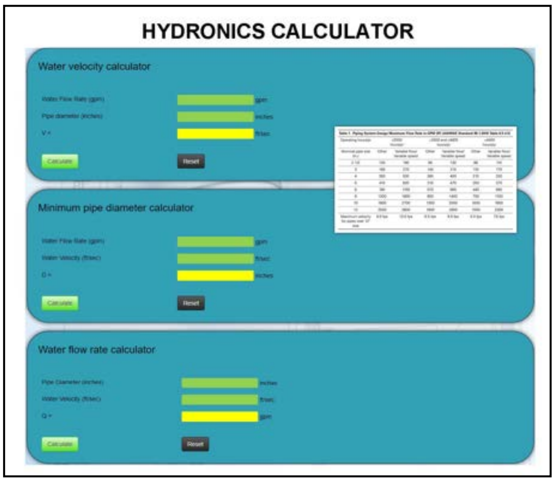
Water Flow Rate through an Orifice Calculator



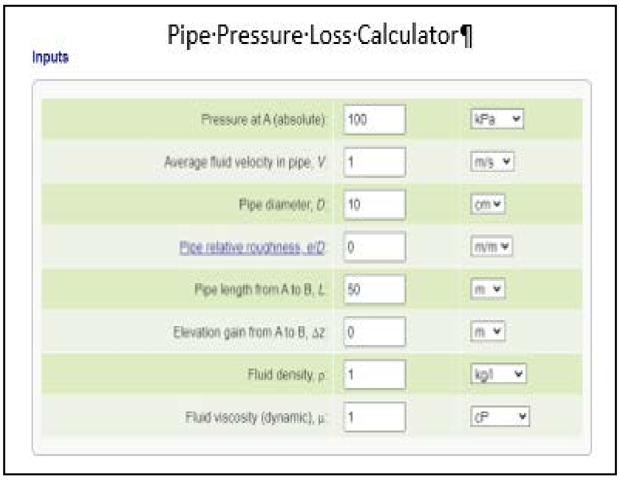
Cubic Feet Calculator



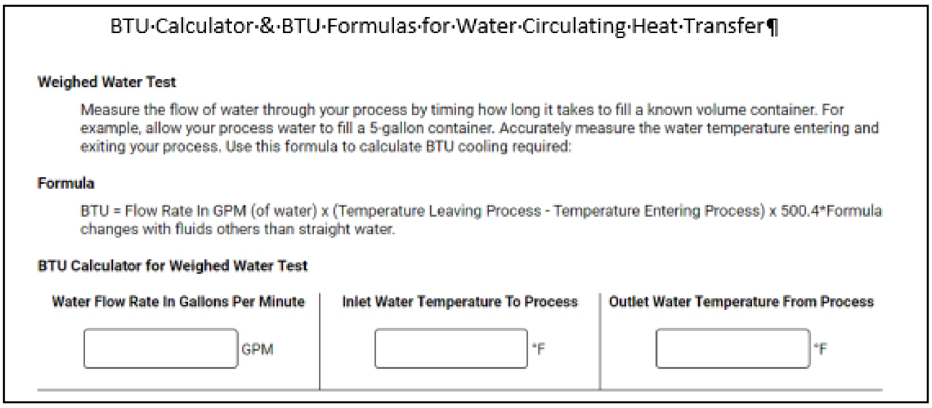
Corrosion Rate Calculator



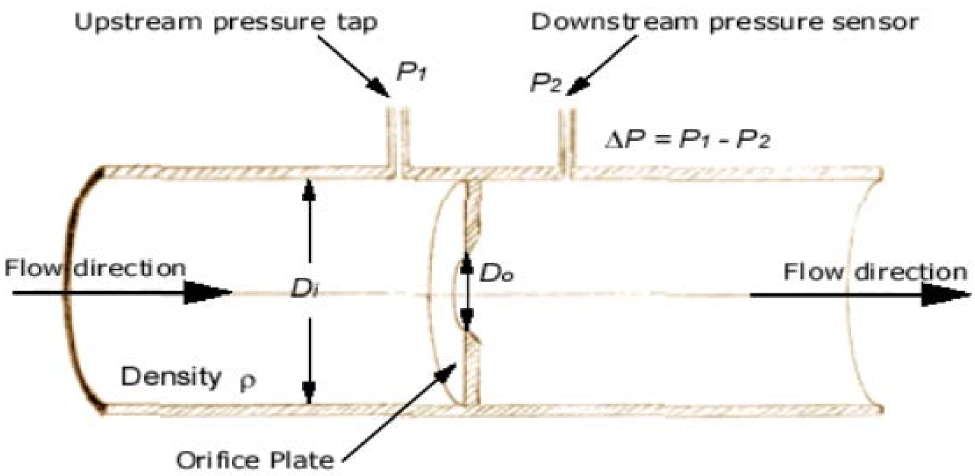
Hydronics Calculator



Pipe Pressure Loss Calculator



BTU Calculator



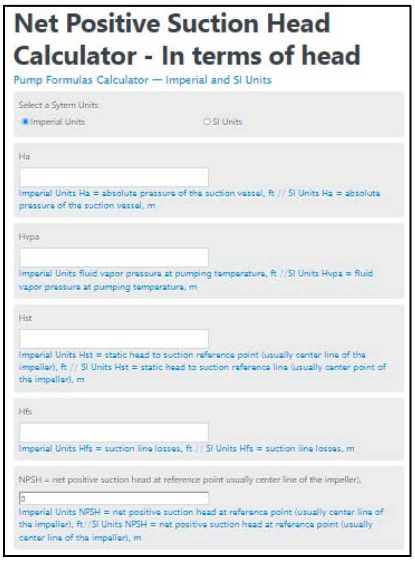
Inputs

Pipe (inlet) diameter upstream of orifice, D_i:	8	in
Orifice diameter (less than the inlet diameter), D_o:	3	in
Pressure difference across the orifice, Δp:	20	psi
Fluid density, ρ:	835	kg/m^3
Flow Coefficient, C_f:	0.82	

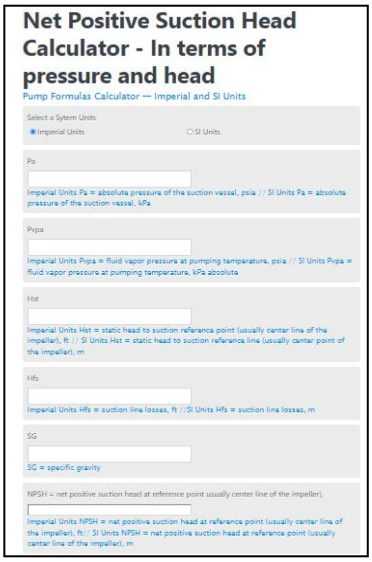
Answers

Velocity at the inlet, V_i:	2.10 m/s	m/s
Volumetric Flowrate, Q:	1080 gpm	gpm
Mass Flowrate:	56.7 kg/s	kg/s

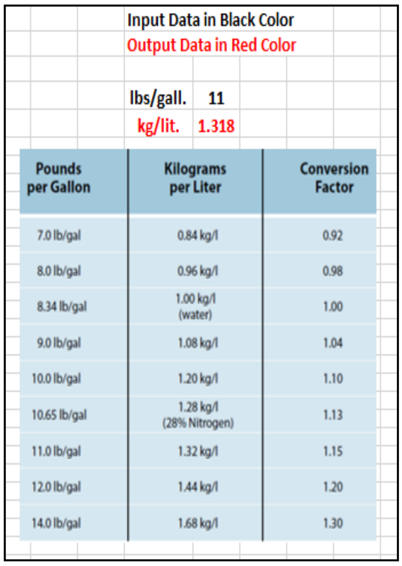
Flow Rate through an Orifice or Valve Calculator



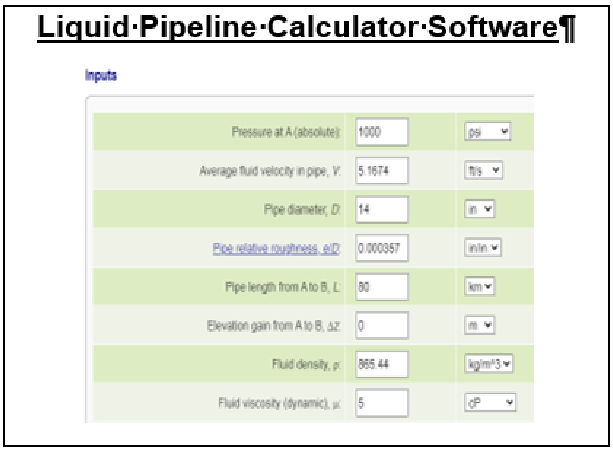
Net Positive Suction Head Calculator



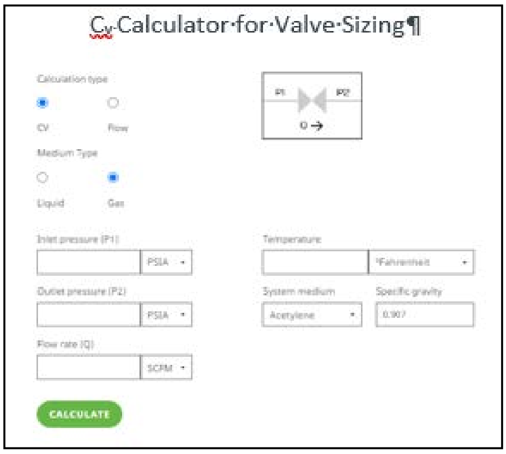
Net Positive Suction Head Calculator



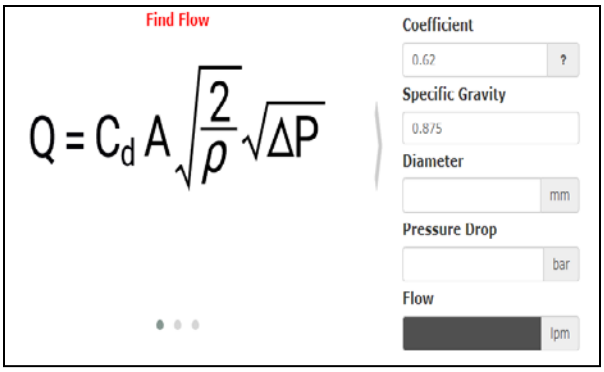
PPG to KG Calculator



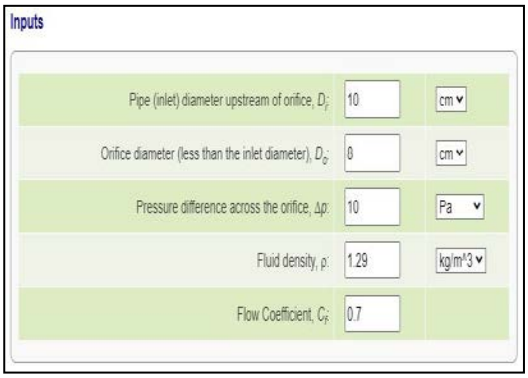
Liquid Pipeline Calculator



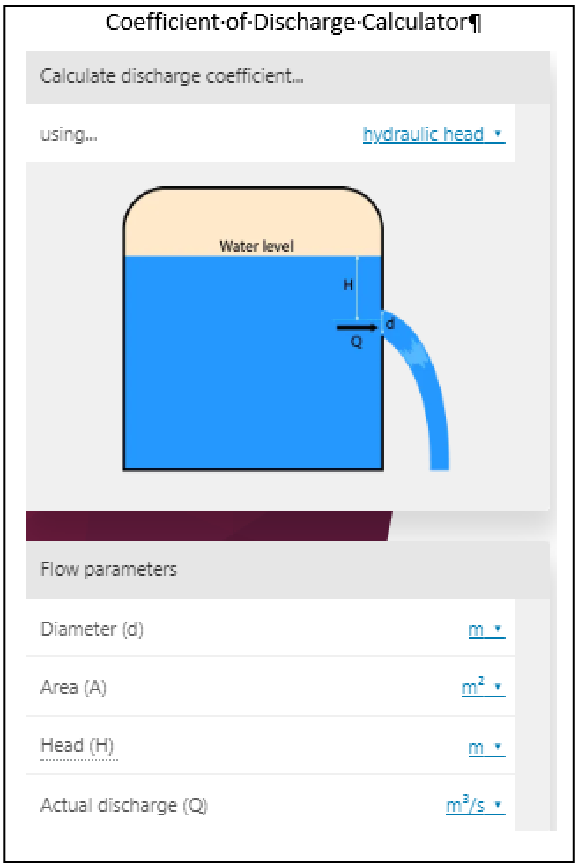
Cv Calculator



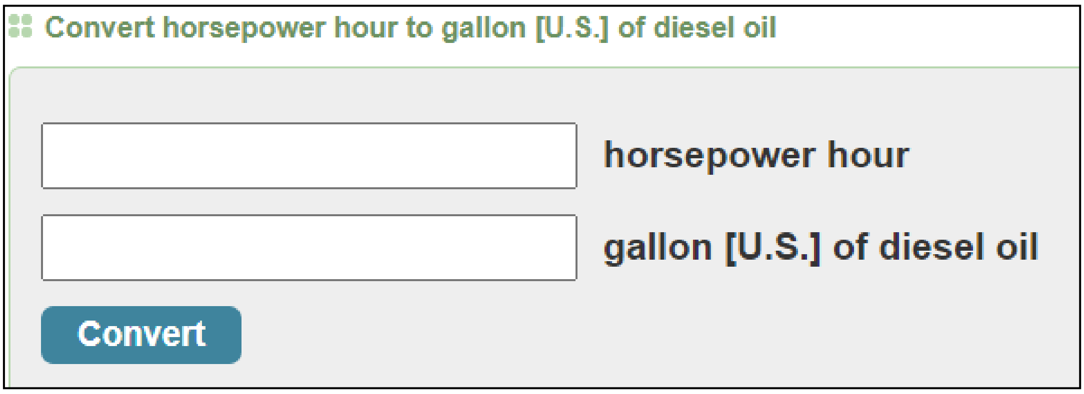
Find Flow Calculator



Flowrate Calculator



Coefficient Discharge Calculator

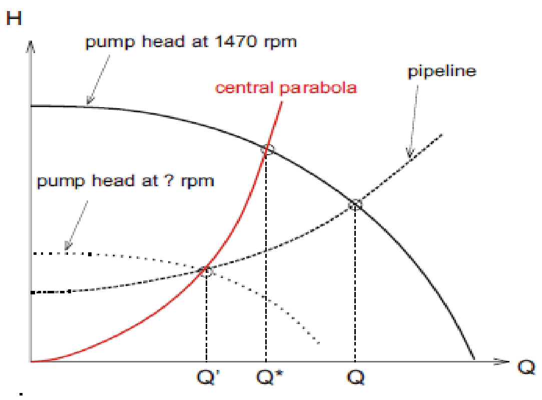


Horsepower Hour Calculator

Liquid Pumping Program	
Input Data	
API	28
c.P.	5
1000 bbl/d	3.3
Length, km	2.4384
I.D., in.	2.800
Rough. (E), in.	0.005
Difference in elev., m	50
Destination press., psi	60
Pump Suc. psi	80
Overall Pump Eff., %	65
Motor Eff., %	90
Motor Loading %	80

Output Results	
Flow Velocity, ft/s	5.0154
Erosion Velocity, ft/s	13.440
E/I.D.	0.001786
sp.gr.	0.8871
Re	19290.3
F	0.02987
Hf, psi	153.67
Hf, m water	108.17
Total Pump Dich. psi	276.68
TDP, psi	196.68
Hydr. Power, HP	16.99
Hydr. Power, Kw	12.67
Shaft Power, HP	18.88
Shaft Power, Kw	14.083
Nama Plate Motor HP	23.60
Nama Plate Motor Kw	17.60

A pump running at $1470[rpm]$ with $H_{pump} = 45 - 2781Q^2$ head delivers water into a pipeline with $H_{pipe} = 20 + 1125Q^2$. Calculate the required revolution number for the reduced flow rate $Q' = 0.05[m^3/s]$.



Solution:

- The actual working point is given by the solution of $H_{pump} = H_{pipe}$, which gives $Q = 0.08[m^3/s]$ and $H = 27.2[m]$.
- Affinity states that while varying the revolutionary speed, H/n^2 and Q/n remain constant. Thus, also H/Q^2 remains constant, let's denote this constant by a. So, while varying the revolutionary speed, the working point moves along the *central parabola* (see figure), given by $H_{ap} = a\,Q^2$.

However, as Q' is given and we also know that this point has to be located on the pipeline characteristic, we know that $H' = 20 + 1125 \times 0.05^2 = 22.81[m]$. Thus, the parameter of the affine parabola is $a = H'/Q'^2 = 9125$.

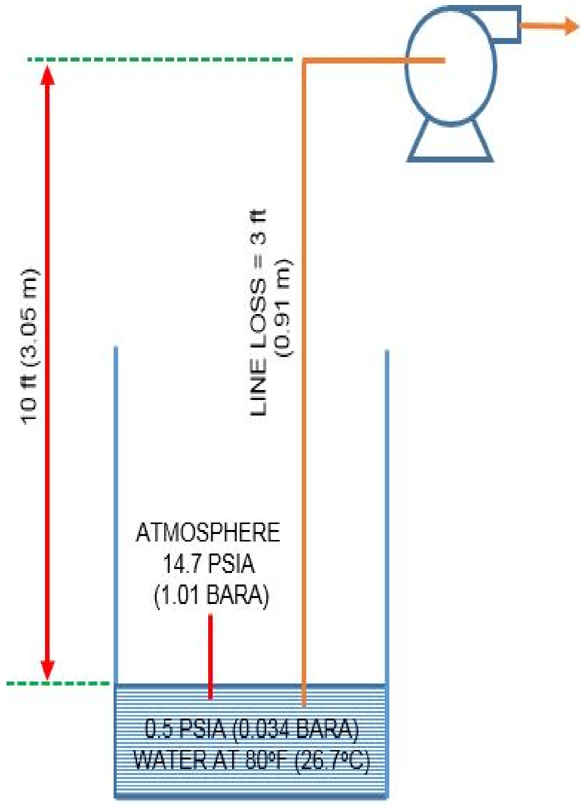
Q^* is given by the intersection of the affine parabola and the original pump characteristic: $H_{ap}(Q^*) = H_{pump}(Q^*)$, which gives $Q^* = 0.06148[m^3/s]$ with $H^* = 34.5[m]$.

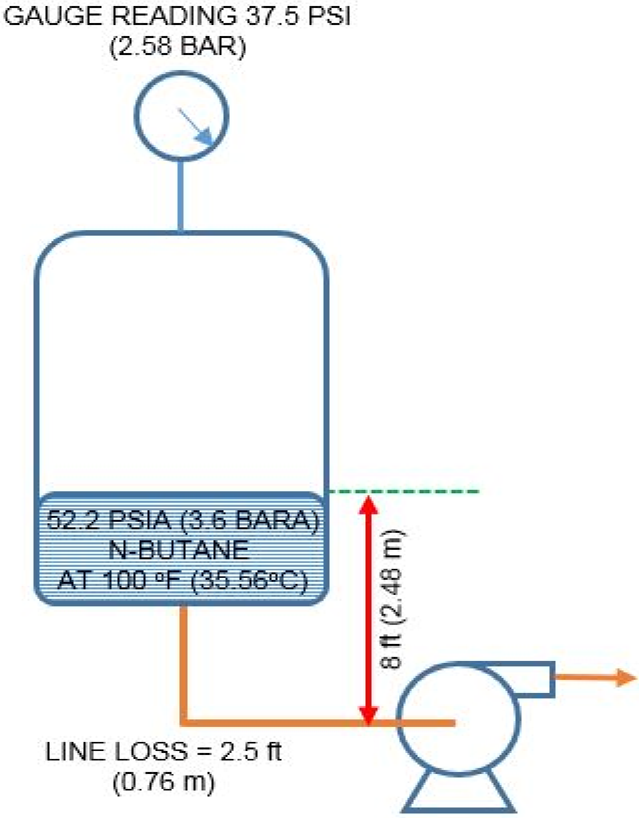
Now we can employ affinity between Q^* and Q':

$$n' = n^* \frac{Q'}{Q^*} = 1470 \times \frac{0.05}{0.06148} = 1195.5[rpm]$$

and just for checking the calculation

$$H' = H^* \left(\frac{n'}{n^*}\right)^2 = 34.5 \times \frac{1195.5^2}{1470^2} = 22.81[m].$$





NPSHA of pump – suction lift

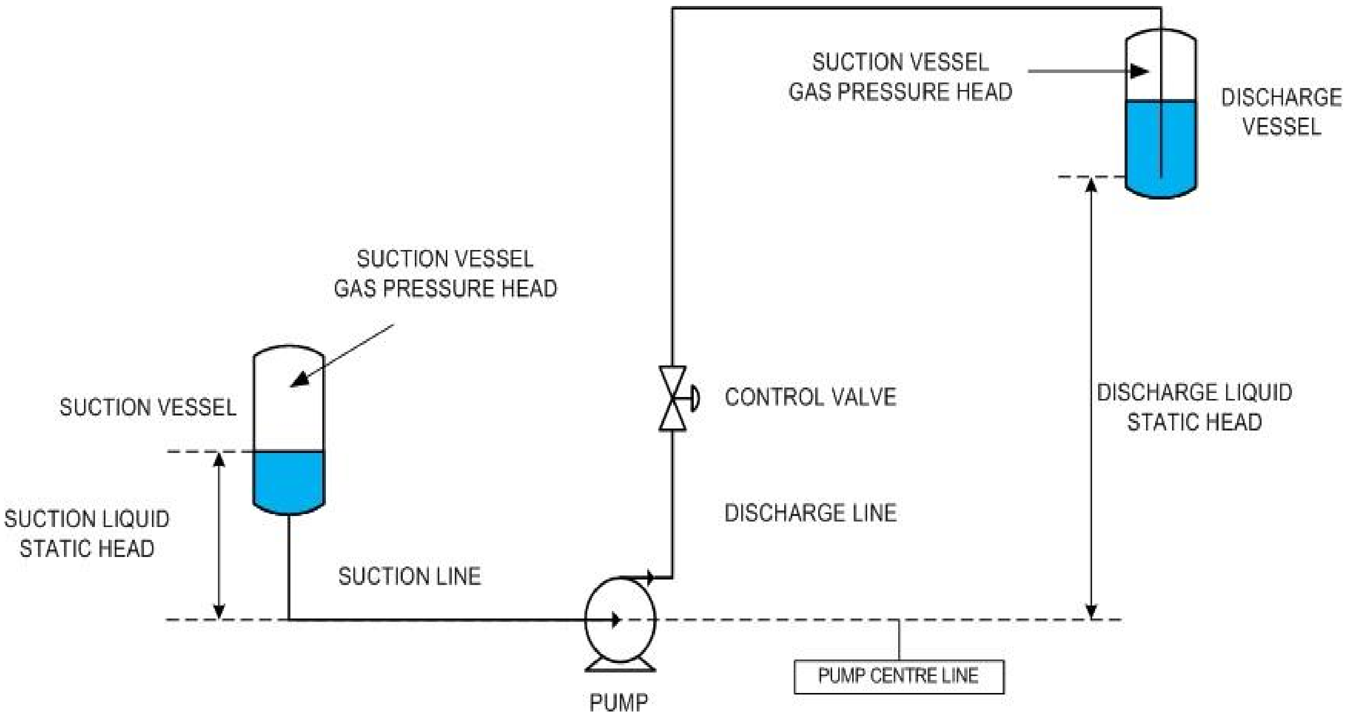
NPSHA of pump – at boiling point
SG of n-butane at 100 deg F = 0.56

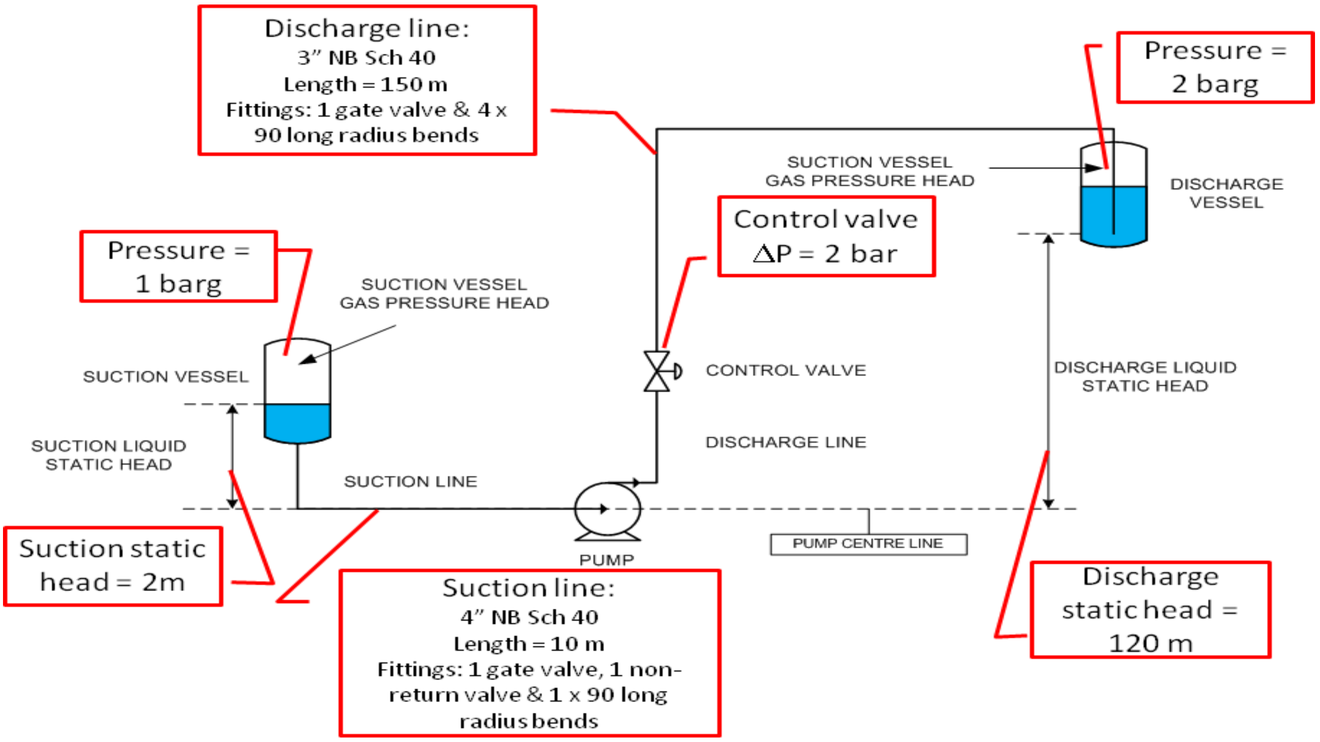
NPSHA = Hatmp.+/- Hs – Hf – Hvap.

https://engineeringunits.com/net-positive-suction-head-calculator/?utm_content=cmp-true

http://www.pressure-drop.com/Online-Calculator/index.html

NPSH Calculations		Output Results	
Input Data		Flow Velocity, ft/s	2.6620
API	36	E/I.D.	0.001671
c.P.	3	sp.gr.	0.8448
Vapor pressure, psi	10	Re	17363.9
Atmp. Pressure, psi	14.7	F	0.0302
Height above pump, ft	20	Hf, psi	0.048
1000 bbl/d	2.0	Hf, ft water	0.111
Length, km	0.003	NPSHA, ft oil	32.72
I.D., in.	2.992	NPSHA, ft water	27.64
Rough. (E), in.	0.005		


SUCTION VESSEL
GAS PRESSURE HEAD
DISCHARGE VESSEL
SUCTION VESSEL
GAS PRESSURE HEAD
SUCTION VESSEL
CONTROL VALVE
DISCHARGE LIQUID
STATIC HEAD
SUCTION LIQUID
STATIC HEAD
DISCHARGE LINE
SUCTION LINE
PUMP CENTRE LINE
PUMP


Discharge line:
3" NB Sch 40
Length = 150 m
Fittings: 1 gate valve & 4 x 90 long radius bends
Pressure = 2 barg
SUCTION VESSEL
GAS PRESSURE HEAD
DISCHARGE VESSEL
Control valve
ΔP = 2 bar
Pressure = 1 barg
SUCTION VESSEL
GAS PRESSURE HEAD
SUCTION VESSEL
CONTROL VALVE
DISCHARGE LIQUID
STATIC HEAD
SUCTION LIQUID
STATIC HEAD
DISCHARGE LINE
SUCTION LINE
PUMP
PUMP CENTRE LINE
Suction static head = 2m
Suction line:
4" NB Sch 40
Length = 10 m
Fittings: 1 gate valve, 1 non-return valve & 1 x 90 long radius bends
Discharge static head = 120 m

Calculator

PUMP DETAILS

Pump tag number		P-001	
Suction vessel tag number		V-001	
Discharge vessel tag number		V-002	
Barometric pressure	P_{atm}	1.013	bara
NPSH available margin	H_{margin}	0	m
Pump efficiency	η	70%	

FLUID PROPERTIES

Fluid		Water	
Phase		Liquid	
Flowrate	m	30000	kg/hr
Density	ρ	998	kg/m3
Viscosity	μ	1	cP
Vapour pressure	P_{vap}	0.023	bara

VESSEL GAS PRESSURES

Suction vessel gas pressure	$P_{suc.\_vessel}$	1	barg
Discharge vessel gas pressure	$P_{dis.\_vessel}$	2	barg

STATIC HEADS

Suction static head	$H_{suc.\_static\_head}$	2	m
Discharge static head	$H_{dis.\_static\_head}$	120	m

PIPELINES

		Suction Line	Discharge Line	
Pipe nominal diameter		4	3	inch
Pipe schedule		Sch 40	Sch 40	
Pipe internal diameter	d	102.26	77.92	mm
Pipe length	L	10	150	m
Absolute roughness	e	0.046	0.046	mm

OUTPUTS

Volumetric flow rate Q 30.060 m3/hr

		Suction Line	Discharge Line	
Relative roughness	e:d	0.00045	0.00059	
Flow area	A	0.00821	0.00477	m2
Velocity	u	1.02	1.75	m/s
Reynolds No.	Re	103758	136170	
Flow regime		turbulent	turbulent	
Friction factor	f	0.02011	0.02010	
Pipe velocity head loss	K_{pipe}	1.966	38.695	
Fittings total velocity head loss	$K_{fittings}$	1.724	2.152	
Frictional pressure loss	$\Delta P_{friction}$	0.02	0.62	bar
Frictional head loss	$H_{friction}$	0.19	6.38	m

Pump suction pressure	$P_{suction}$	2.19 bara
Pump suction head	$H_{suction}$	22.37 m
Pump discharge pressure	$P_{discharge}$	15.39 bara
Pump discharge head	$H_{discharge}$	157.16 m
Net positive suction pressure available	P_{NPSHA}	2.17 bara
Net positive suction head available	NPSHa	22.13 m
Pump total differential pressure	ΔP_{pump}	**13.20 bar**
Pump total differential head	H_{pump}	**134.79 m**
Pump absorbed power	E	**15.74 kW**

Results of above calculations may be confirmed through either of followinglinks:

https://www.swagelok.com/en/toolbox/cv-calculator

https://experttoolsonline.com/danfoss/orifice_calculator

https://www.efunda.com/formulae/fluids/calc_orifice_flowmeter.cfm

https://www.omnicalculator.com/physics/coefficient-of-discharge

Power Calculations: *https://inventory.powerzone.com/resources/centrifugal-pump-power-calculator/%3Aflu%3DGPM%3Apru%3DHEAD%20FT%3Apu%3DHP*

http://irrigation.wsu.edu/Content/Calculators/General/Required-Water-Pump-HP.php

Required Compressor Horsepower
https://www.engineeringtoolbox.com/horsepower-compressed-air-d_1363.html

Input Data	
T1, F	60
K	1.35
P1, psi	14.7
P2, psi	500
Gas sp.gr.	1
No. of Comp. stages	3
Gas million SCMD	1.5
Eff. of Gas Comp., %	85
Eff. of Driving Motor, %	90

Output Results	
Compression Ratio	34.014
Cp, J/kg/K	1107
Gas, cfm	36791.50
Gas, kg/s	21.250
Theoretical Power, HP	9731.847
Total Required HP	12721.37

Heater Duty
https://www.advantageengineering.com/fyi/288/advantageFYI288.php

Input Data	
Million BTU/hr.	0.75
API	10.0
Specific Heat, BTU/lb/F	1.00
Delta Temp., F	60
Heater Eff., %	100

Output Results	
Delta Temp., C	15.6
Mega Watt	0.220
Billion Joule/hr.	0.791
gpm	25.0
gallon/hr.	1498.4
Lit./min.	94.5
m3/hr.	5.7
1000 bbl/d	0.856
Required Diesel Lit./day	502.90
Required Diesel bbl/d	3.16
Required Gas, 1000 ft3/d	16.364
Required crude oil, bbl/d	3.268

https://www.enggcyclopedia.com/2011/09/problem-solving-heat-exchanger-tubeside-pressure-drop-calculation/

Input Data		Output Results	
Mass Flow Rate, kg/hr.	2000.0	cm3/s	562.303
Fluid Density, Kg/m3	988.0	V, cm/s	110.9720
Visc., c.P.	0.53	Re	52544.59
Pipe Diameter (D), in.	1	f	0.0261
Roughness (E), mm	0.045	Total Hf, cm (per single tube)	22.5583
Tube Length, m	3.5	Total Hf, psi (per single tube)	0.3166
No. of tubes	1	Total Hf, bar (per single tube)	0.0218

Heat exchanger tube side pressure drop calculation

Calculate the tube side pressure drop for the following heat exchanger specification,

Process fluid = water

Inlet pressure = 4 barg

Inlet temperature = 50^0C

Outlet temperature = 30^0C

Tubeside flowrate = 50000 kg/hr

Number of tubes = 25

Tube ID (internal diameter) = 1 inch

Tube length = 3.5 m

Total volumetric flow = 50000 kg/hr ÷ 988.0 kg/m^3 = 50.61 m^3/hr Volumetric flow in each 1" tube = 50.61 ÷ 25 = 2.02 m^3/hr Pressure loss per unit length of the tube is then calculated using EnggCyclopedia's pressure drop calculators for pipes and tubes. This calculator is based on Darcy-Weisbach equation.

Pressure loss across a single tube (ΔP/L) = 6.17 bar/km

SINGLE PHASEFLOW INPUTS

W – Mass flow capacity	2000	kg/h
ρ – Density of fluid	988	kg/m^3
μ – Viscosity of fluid (either liquid or gas)	0.53	cP

PIPE SPECIFICATIONS

e – Effective roughness of the pipe	0.045	mm
d – Nominal diameter of the pipe	1	inches
sch – pipe schedule	STD	

Calculate pressure loss | Reset

RESULTS

Fluid Velocity	1.110	m/s
Volumetric flow	2.02	m^3/hr
Reynold's No.	52557.9	
Pressure loss	6.1715	bar/km

Tube length (L) = 3.5 m

Tubeside pressure drop (ΔP) = 6.17 × 3.5 / 1000 = 0.0216 bar

Another alternative is to directly use EnggCyclopedia's Heat Exchanger Tube side Pressure Drop Calculator. All the inputs given in the sample problem statements are given to the calculator and pressure drop across the tubeside is calculated as output. This calculator uses the same basic steps discussed above and hence the answer also matches with the figure above (0.0216 bar) . The following image is a snapshot of this direct calculation of tubeside pressure drop.

Exchanger tubeside pressure drop

Tubeside inputs		
Total tubeside mass flow	50000	kg/hr
Tubeside Density	988	kg/m^3
Tubeside Viscosity	0.53	cP
Number of tubes	25	
Total tube length (accounting for all tube passes)	3.5	m
Tube nominal diameter	1	inches
Tubeside roughness	0.045	mm
Calculate pressure drop	Reset	
Results		
Tubeside pressure drop	0.0216	bar

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